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(54) **Polyamide compositions.**

(57) Novel crystalline copolymers and terpolymers having high heat deflection temperatures are prepared from hexamethylene diamine and either mixtures of terephthalic acid and adipic acid or mixtures of terephthalic acid, isophthalic acid and adipic acid.

**EP 0 291 096 A2**

## POLYAMIDE COMPOSITIONS

Background of the Invention

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Field of the Invention

10 The field of this invention relates to crystalline copolyamides or terpolyamides from hexamethylene diamine (HMDA) and either mixtures of terephthalic acid (TA) and adipic acid (AA) or mixtures of TA, isophthalic acid (IA) and AA.

Properly filled compositions from HMDA and TA, AA and HMDA and TA, IA, and AA having heat deflection temperatures in excess of about 240 to 350° C are unknown to the prior art. Likewise, processes for making crystalline copolyamides from HMDA and the aforementioned diacids giving polymers of injection moldable quality have not been contemplated in the prior art.

References of interest include U.S. Patent 3,553,288, which discloses polyester blends, some components of which can be TA, IA or AA. U.S. Patent 4,218,509 discloses various fibers. Transparent terpolyamides from TA, IA, AA and HMDA moieties are disclosed in Japanese Patent J7021116. British Patent Application 604/49 discloses isomorphous TA, AA-HMDA polyamides; German Offenlegungsschrift 2,651,534 discloses fiber-forming random terpolyamides including TA and IA and very small amounts of AA with HMDA; Japanese Kokai J71018809, J52085516 and J71028218 disclose fibers from TA, IA, AA and HMDA polyamides. Other references include U.S. Patent 3,551,548 which discloses amorphous polyamides, U.S. Patent 3,526,524 which relates copolyamines from adipic acid and U.S. Patent 4,238,603 which relates to amorphous fibers which can be crystallized after the essentially draining amorphous fiber is heat treated at temperatures above the glass transition temperature. In reviewing all these references it is clear that crystalline copolyamides manufactured from HMDA and mixtures of TA and AA or HMDA and mixtures of TA, IA and AA including filled compositions of these polymers having heat deflection temperatures of about 240 to about 305° C and having a molecular weight about 5,000 to about 40,000 and having tensile strengths of about 20,000 psi to about 40,000 psi have not been contemplated by the prior art.

30 The general object of this invention is to provide molding compositions reinforced with glass fibers, glass beads, minerals or a mixture thereof made from polyamides derived from HMDA and mixtures of TA and AA or from HMDA and mixtures of TA, IA and AA. Other objects include a process for the manufacture of the crystalline polyamide and catalysts for the polycondensation reaction and fibers made from the polyamides.

35 We have now found that filled molded copolyamides can be obtained from HMDA and mixtures of TA and AA or from HMDA and mixtures of TA, IA and AA. The mole ratio of HMDA to TA to AA can be in the range of about 100/65/35 to about 100/95/5. The preferred range of HMDA to TA to AA is about 100:65:35 to about 100:80:20. The mole ratio of HMDA:TA:IA:AA is about 100:60:20:20 to about 100:90:5:5. The preferred ratio of HMDA:TA:IA:AA is about 100:65:25:10 to about 100:80:5:15. The crystalline polyamides, when filled and molded with glass fiber, glass beads, minerals or a mixture thereof have a heat deflection temperature in the range of about 240 to about 305° C, as determined by ASTM Method D648. This is an unusual feature and completely unexpected from the prior art since comparable polyamides have much lower heat deflection temperatures. The importance of having high heat deflection temperatures is that it enables the injected copolyamides to be used in applications such as the hood of an automobile, shroud for a lawn mower, chain saw guard, and in electrical connector applications. In addition to the high heat deflection temperature, the tensile strength of these copolyamides is about 20,000 to about 40,000 psi which is as high or higher than that of die cast aluminum or zinc while the specific gravity of our copolyamides is about one-half of that of aluminum or zinc. Thus, these copolyamides are particularly useful in transportation equipment applications. These filled copolyamides also have a flexural modulus in excess of about 1,000,000 to about 3,000,000 psi as determined by ASTM Method D790. This property is advantageous in applications requiring dimensional stability. The molecular weight of copolyamides is about 5,000 to about 40,000.

Our copolyamide composition can be filled with about 10 to about 80 weight percent glass fibers, glass beads, minerals, or a mixture thereof, or graphite fibers. Advantageously, the molding composition may contain from about 20 to about 50 weight percent of glass fibers, glass beads, minerals, or a mixture

thereof, or graphite fibers. Our studies have shown that high heat deflection temperatures and also the cost of molding products derived from copolyamides can be reduced by substituting for part of the polymer about 10 to about 60 weight percent thereof with glass fibers, glass beads, minerals, or graphite fibers. These glass filled copolyamides are much more economical than molding compositions prepared without the use of the glass fibers, glass beads, minerals, or graphite fillers. The use of polyimides and amides as engineering plastics has been limited only by their relatively high cost. Thus, employing our invention, through which the inherent cost can be brought down, the commercial application of polyamides requiring very high flexural strength can be greatly expanded.

We have prepared monofilaments using our novel polyamides. The process starts with a single screw extruder to supply a melt for conversion to fiber. The die for monofilament is similar to the multifilament die. The monofilament process is a slower operation, typically 50 to 200 feet/minute. For the melt spinning operations, 40 to 80 feet/minute was the speed used for the monofilament processing. The monofilament, on the other hand, is water quenched with much less melt draw down. The monofilament is subsequently drawn with heated drawing systems. The monofilament drawing is done in-line using heating ovens.

Suitably, in our processes for the manufacture of polyamides, the production can be divided into the prepolymer and final polycondensation sections. The prepolymer section may be batch, batch-continuous or fully-continuous and consists of one or more stirred tank reactors of suitable design. The prepolymer product of this stage is a polyamide oligomer with an inherent viscosity (60/40 phenol/TCE, 30°C) of 0.1 to 0.2 dl/g.

Batch production of prepolymer may be carried out in any suitably designed stirred reactor which can process materials of high viscosity. Feed materials consisting of diacids (TA, IA, and AA in the desired ratios), HMDA and additives are charged to the reactor at 175°F. Water content of the resulting solution should be no more than 15% by weight. Temperatures are then raised to 500 to 600°F as quickly as possible.

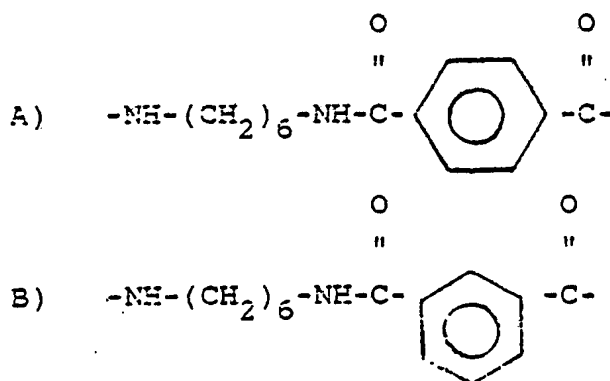
Table 1  
Terpolyamide Monofilament

Sample	T <sub>m</sub>	Melt	Denier	Elongation
<u>TA/IA/AA-HMDA</u>	<u>(C°)</u>	<u>Temp</u>	<u>(g/9000m)</u>	<u>(%)</u>
Composition				
65/25/10-100	310	334		
		340	650	9.2
			~900	~11.5
			1050	21.3
Tenacity		Initial		Draw
<u>(g/d)</u>		<u>Modulus</u>		<u>Ratio</u>
4.0		<u>(g/d)</u>		<u>(X:1.0)</u>
~5.8		56.0		4.4
3.6				5.2
		54.7		5.2

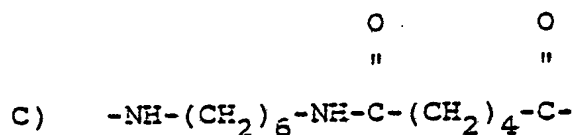
Pressures are allowed to build to the limits of the equipment. After the target temperature is reached, the pressure is reduced to atmospheric over a period of 5 to 120 minutes. The polymer is then allowed to flow

out of the reactor and is caught under an inert gas blanket. The prepolymer is then ground and fed to the final polycondensation section.

Our novel injection moldable crystalline polyamide copolymers of HMDA and TA, IA and AA comprise the following recurring structural units:



and



In the case of the HMDA, TA, AA copolyamides the structure is composed only of A and C moieties. The molar ratio of A:C units is about 40:60 to about 90:10. The injection molding of our copolyamides is accomplished by injecting the copolyamide into a mold maintained at a temperature of about 100 to 200 °C. In this process, a 20-second to 1-minute cycle is used with a barrel temperature of about 300 to 350 °C. These temperatures will vary depending on the T<sub>g</sub> and T<sub>m</sub> of the polyamide being molded. These copolyamides have excellent heat deflection and other physical properties.

The addition of reinforcing materials, particularly the physical properties such as flexural strength, is improved if the copolyamides contain from about 10 to about 60 percent by weight glass fibers, glass beads, minerals, or mixtures thereof. In the preferred range, the copolyamides contain about 20 to about 50 percent by weight of glass fibers, glass beads, or graphite, or mixtures thereof. Suitably, the reinforcing materials can be glass fibers, glass beads, glass spheres, or glass fabrics. The preferred fillers are glass fibers. These are made of alkali-free boron-silicate glass or alkali-containing C-glass. The thickness of the fibers is suitably, on the average, between 3mm and 30mm. It is possible to use long fibers in the range of from 5mm to 50mm and also short fibers with each filament length of 0.05mm to 5mm. In principle, any standard commercial grade fiber, especially glass fibers, may be used. Glass fibers ranging from 5mm to 50mm in diameter may also be used as a reinforcing material.

The reinforced polyamide polymers may be prepared by any conventional method. Suitably, so-called roving endless glass fiber strands are coated with the polyamide melt and subsequently granulated. Advantageously, the cut fibers and glass beads may also be placed with granulated copolyamides and the resulting mixture melted in a conventional extruder, or alternatively, the fibers may be determined, introduced into the copolyamides, and melted through a suitable inlet in the extruder. The injection molding conditions are given in Table 2 below.

Table 2

Mold Temperature 100° to 200° C  
 5 Injection Pressure 6,000 to 15,000 psi and held for 10 to 20 seconds  
 Back Pressure 100 to 1,000 psi  
 Cycle Time 20 to 60 seconds  
 Extruder

Nozzle Temperature 320° to 340° C  
 10 Barrels  
 Front Heated to 300° to 350° C  
 Screw 20 to 60 revolutions/minute

The following examples illustrate the preferred embodiment of this invention. It will be understood that the examples are for illustrative purposes only and do not purport to be wholly definitive with respect to the conditions or scope of the invention.

Our preferred process for prepolymer production utilizes four major units. These are the salt reactor, the surge and aging vessel and the first polycondensation reactor. Steam, advantageously, is used for pressure control on the first three stages. Steam use is helpful, since we can control the extent of the reaction without worrying about unknown pressure leaks. Steam is also useful to our process, since we use no water or low amounts of water in our feed material. When pressure make-up is required, use of nitrogen or other inert gas can cause a reduction in water partial pressure and a release of water from the salt. When the operating pressure is greater than the equilibrium steam partial pressure at operating temperatures, it will be advantageous to use an inert gas in addition to steam. In prior art processes, steam comes from the excess water in the feed, but in our novel process the extra water will be generated by the polycondensation reaction.

Feed materials can suitably be introduced to the first stage of our process, the salt reactor, in any of several ways. For example, pre-weighed charges can be fed to the salt reactor via lock hoppers. Another suitable procedure is a slurry feed of the HMDA and diacids. This has the advantage of putting the batch stage into less expensive equipment and reduces negative effects of cyclic operation on the first two stages. It also would allow easy analysis of feeds prior to its introduction into the process. Advantageously, the reactants can be charged as a paste via an extruder. Such a feed system could preheat the feed materials and would allow a minimal water level in the feed. The primary limitation of this system is that high temperature analytical equipment must be employed.

The salt reactor is a stirred tank reactor agitated by downward flowing pitched blade turbines. Impeller speed should be great enough to keep solids suspended until reacted. Pressure capability should be enough to prevent volatilization of the lowest boiling monomer component. Free water levels in the salt reactor can range from 0 percent (anhydrous feed materials) to about 25 to 30 percent. This is governed by feeding requirements and by phase equilibrium demands. Small amounts of water provide significant freezing point depression and improve processability of the various high melting salts.

The second vessel is a surge or aging vessel. It is at the same pressure and temperature as the salt reactor. It serves two functions. It translates the batch operation of the salt reactor to continuous operation when lock hopper feeding is used. It also allows the salt additional residence time to form fully and stabilize. The second stage also minimizes the possibility that unreacted monomer could pass through to the polycondensation reactor. The surge reactor can be non-agitated, but potential problems with gel justify the use of an agitated reactor. The surge or aging vessel may be eliminated when a continuous feed system is provided.

The third stage of our process is the first polycondensation reactor. This reactor is a continuous stirred tank reactor and has a reduced pressure and an increased temperature over the two prior reactors. This reactor can be agitated by either a pitched blade turbine or a helical anchor. A helical anchor permits higher product viscosities and improved productivity in our final extruder reactor. An important factor in the success with our novel process had been control of melt rheology in the first polycondensation reactor by keeping inherent viscosity low. This concept allows us to minimize gel and polymer build-up problems in the first polycondensation reactor, but it does force more work on the finishing reactor. The balance between the first polycondensation reactor and the extruder will vary for each different resin just as the water level requirements in the feed will vary.

The final polycondensation stage of the process is a twin screw extruder reactor. The twin screw extruder is an advantageous component in our process as it allows us to easily handle the stiff, high melting

point resins that we manufacture. Other types of finishing reactors such as disk ring reactors, agitated stranding devolatilizers, and thin film evaporators can be utilized; however, some of these may have difficulty in handling the high viscosity of our resins. The inherent viscosity (I.V.) is measured in 60/40. phenol/tetrachloroethane at 30° C.

Table 3

A. Terpolyamide 65/25/10 (TA/IA/AA)-HMDA

Process Conditions	Salt Reactor	Transition Reactor
Pressure (PSIG)	450	425
Temperature °F	450	450
Residence Time (min.)	---	---
I.V. (dl/g)	---	---

A. Terpolyamide 65/25/10 (TA/IA/AA)-HMDA

Process Conditions	1st Polycond. Reactor	ZSK-30 Extruder
Pressure (PSIG)	350	atm.
Temperature (°F)	460	670
Residence Time (min.)	30 min.	2 min.
I.V. (dl/g)	0.12	1.25

B. Terpolyamide 75/15/10 (TA/IA/AA)-HMDA

Process Conditions	Salt Reactor	Transition Reactor
Pressure (PSIG)	450	450
Temperature (°F)	440	415
Residence Time (min.)	---	---
I.V. (dl/g)	---	---

B. Terpolyamide 75/15/10 (TA/IA/AA)-HMDA

Process Conditions	1st Polycond.	ZSK-30
	Reactor	Extruder
Pressure (PSIG)	365	---
Temperature (°F)	460	690
Residence Time (min.)	30 min.	2 min.
I.V. (dl/g)	0.12	1.0

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Catalyst can suitably be employed in our process. These catalysts include the following compounds:  $\text{NaH}_2\text{PO}_2$ ,  $\text{H}_3\text{PO}_2$ ,  $\text{H}_3\text{PO}_4$ ,  $\text{H}_2\text{SO}_4$ ,  $\text{HCl}$ ,  $\text{Na}_3\text{PO}_3$ ,  $\text{NaH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$ . The amount of catalyst present can vary from about 0.01 to about 0.2 weight percent of the total weight of the reactants.

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Table 4  
MECHANICAL PROPERTIES OF 45% GLASS-FIBER FILLED  
POLYAMIDES AND TWO DIE CAST METALS AT  
ROOM TEMPERATURE

Sample	Tensile		
	Strength	Elongation	
	ASTM Method	ASTM Method	
	D638	D638	
	M psi	%	
Nylon 6,6.	33.0	5.5	
Die cast Mg.	34.0	~8.0	
Die cast Al	35.0	~9.0	
65/25/10	37.0	5.1	
75/15/10	38.7	4.8	
65/25/10 (60% GF)	40.2	4.8	

Sample	Flexural		Notched
	Strength	Modulus	Izod
	ASTM Method	ASTM Method	ASTM Method
	D790	D790	D256
	M psi	MM psi	ft-lb/in
Nylon 6,6	50.3	1.84	3.4
Die cast Mg	-	6.50	-
Die cast Al	-	10.00	-
65/25/10	51.5	1.85	3.4
75/15/10	55.3	2.46	3.4
65/25/10 (60% GF)	59.0	2.43	4.9
Moldability:	Good, shorter cycle time and lower mold shrinkage than Nylon 6,6		



Table 4 (Cont'd.)

	Tensile		HDT	Water Absorption %
	Impact		(at 264 psi)	
	ASTM Method		ASTM Method	
	D638		D648	
<u>Sample</u>	<u>ft-lb/in<sup>2</sup></u>	<u>°F</u>		
Nylon 6,6	97	493		0.65
Die cast Mg	-	-		-
Die cast Al	-	-		-
65/25/10	136	574		0.21
75/15/10	100	>580		0.15
65/25/10 (60% GF)	128	578		0.21

Moldability: Good, shorter cycle time and lower mold shrinkage than Nylon 6,6

Table 5

MATERIAL PROPERTIES OF REINFORCED AND  
75/15/10 TA/IA/AA TERPOLYAMIDE

	Tensile		Tensile	
	Strength		Elong.	
	ASTM Method		ASTM Method	
	D638		D638	
<u>Sample</u>	<u>Graphite Fiber %</u>	<u>Glass Fiber %</u>	<u>M psi</u>	<u>%</u>
75/15/10	25	25	28.1	3.0
75/15/10	0	45	38.7	4.8

Table 5 (Cont'd)

Sample	Flexural Strength	Flexural Modulus	Notched Izod
	ASTM Method	ASTM Method	ASTM Method
	D790	D790	D256
	M psi	MM psi	ft-lb/in
75/15/10	41.6	2.74	1.6
75/15/10	55.3	2.46	3.4

Sample	HDT (at 264 psi)	Water Absorp.
	ASTM Method D648	
	°F	%
75/15/10	580	0.24
75/15/10	580	0.15

Table 6

MATERIAL PROPERTIES OF 65/25/10 TA/IA/AA  
TERPOLYAMIDE AT HIGH TEMPERATURES

Testing Temperature °F	Glass Fiber %	Tensile	
		Strength	Elongation
		ASTM Method	ASTM Method
		D638	D638
		M psi	%
65/25/10 TA/IA/AA Terpolyamide (no annealing required)			
73	45	37.5	5.1
300	45	12.9	7.2
500	45	9.1	7.5

Table 6 (Cont'd.)

Testing Temperature °F	Flexural	
	Strength	Modulus
	ASTM Method	ASTM Method
	D790	D790
	M psi	MM psi
73	50.1	1.70
300	20.2	0.91
500	13.0	0.65

Table 7

MECHANICAL PROPERTIES OF 45% GLASS-FIBER FILLED  
65/25/10 TA/IA/AA TERPOLYAMIDE AGED AT 400°F

0 hour at 400°F					
Irganox 1098 %	Ten. Str.	Ten. Elong.	Flex. Str.	Flex. Mod.	
	ASTM Method	ASTM Method	ASTM Method	ASTM Method	
	D638	D638	D790	D790	
	M psi	%	M psi	MM psi	
0	32.3	4.2	46.1	1.77	
1	29.5	4.5	43.5	1.78	
600 hours at 400°F					
0	15.5	2.3	23.9	1.61	
1	25.7	3.5	33.8	1.78	
1000 hours at 400°F					
0	10.2(32%)	1.7(41%)	10.5(22%)	1.06(60%)	
	18.2(63.4%)	2.8(62.2%)	32.1(73.8%)	1.73(97%)	

Table 8  
MATERIAL STRENGTH OF 65/25/10 TA/IA/AA  
TERPOLYAMIDE LAMINATES

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		<u>Compression molding</u>	
		<u>Temp.</u>	<u>Pressure</u>
12 layers	8 layers		
Glass	Graphite		
<u>% Wt</u>	<u>% Vol</u>	<u>°F</u>	<u>psi</u>
65/25/10 TA/IA/AA Terpolyamide			
71	-	655	600
-	60	650	600
-	60	655	600

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<u>Flexural</u>		<u>Horizontal</u>
<u>Strength</u>	<u>Modulus</u>	<u>Shear</u>
<u>ASTM Method</u>	<u>ASTM Method</u>	<u>ASTM Method</u>
D790	D790	D638
<u>M psi</u>	<u>MM psi</u>	<u>M psi</u>
65/25/10 TA/IA/AA Terpolyamide		
109.3	4.47	9.19
130.0	9.66	9.76
137.0	9.87	9.80

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Table 9  
MATERIAL PROPERTIES OF 45% GLASS-FIBER FILLED NYLON  
6,6 and 65/25/10 TA/IA/AA TERPOLYAMIDE

	Tensile Strength	Tensile Elong.	Flexural Strength
	ASTM Method	ASTM Method	ASTM Method
	D638	D638	D790
<u>Sample</u>	<u>M psi</u>	<u>%</u>	<u>M psi</u>
1. ASTM Standard Condition			
Nylon 6,6	33.0	5.5	50.3
65/25/10	37.9	5.1	51.5
2. After 1000 hours of water immersion			
Nylon 6,6	20.9 (63%)	4.9 (89%)	29.1 (57%)
65/25/10	25.9 (68%)	3.6 (70%)	41.1 (80%)
3. Equilibrium Condition			
Nylon 6,6	17.5	5.5	26.5
(2600 hours of water immersion)			

	Flexural Modulus	HDT (at 264 psi)	Water Absorp.	Dimens. Change
	ASTM Method	ASTM Method		
	D790	D648		
<u>Sample</u>	<u>MM psi</u>	<u>°F</u>	<u>%</u>	<u>%</u>
1. ASTM Standard Condition				
Nylon 6,6	1.84	493	0.65	0.04
65/25/10	1.85	574	0.21	0.00
2. After 1000 hours of water immersion				
Nylon 6,6	0.95 (51%)	480	3.31	0.14
65/25/10	1.79 (97%)	571	0.99	0.05
3. Equilibrium Condition				
Nylon 6,6	0.88	464	4.76	0.24
(2600)				
65/25/10			1.43	0.08
(2600 hours of water immersion)				
65/25/10 (55% glass fiber-2600 of water immersion)			1.08	0.02

## Example A

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65/25/10/100 TA/IA/AA/HMDA parts by molar ratio Terpolyamide:

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The reactants are loaded into the 4CV Helicone reactor which has been preheated to 200°-300° F. The temperature control is set at 605° F. The agitator is at the maximum speed (47 rpm). The reactor pressure rises to 120 psi in 16 minutes. The melt temperature is 438° F. The reactor pressure is controlled at 120 psi for 5 minutes as the melt temperature rises to 471° F. The reactor pressure is then vented to 100 psi over a two-minute period. The reactor pressure is controlled at 100 psi until the melt temperature reaches 580° F. The reactor is then vented to atmospheric pressure over a six-minute period. A slow nitrogen sweep is applied to the reactor. The melt temperature reaches 609° F after 5 minutes at atmospheric pressure. The reaction is then stopped. The resin I.V. is determined to be 1.35 dl/g. The run time is 50 minutes.

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Table 10  
MECHANICAL PROPERTIES OF TERPOLYAMIDE

5	Run Number	<u>4CV31</u>	<u>4CV37</u>
	TA/IA/AA Mole Ratio	55/15/30	65/25/10
	Run Time, minutes	115	47
10	Capping Agent, mole % <sup>a</sup>	2BA	None
	Water <sup>b</sup>	Yes	None
	Stabilizer <sup>c</sup>	None	Yes
15	Resin I.V., dl/g	1.12	1.36
	Tensile Strength		
	ASTM D638		
20	At Yield, psi	d	15,000
	At Break, psi	12,800	13,900
	Tensile Elongation		
	ASTM D638		
25	At Yield, %	d	7.8
	At Break, %	4.4	132
	Flexural Strength, psi	---	21,500
30	ASTM D790		
	Modulus, psi	457,000	447,000
	Notched Izod, ft-lb/in	0.7	1.2
	ASTM D256		
35	HDT at 264 psi, °F	194	226
	ASTM D648		
	Tensile Impact, ft-lb/in <sup>2</sup>	39	136
40	ASTM D638		

a. BA = benzoic acid.

b. If yes, 225.6 grams of deionized water were used for the batch.

c. If yes, 0.08% sodium hypophosphite was used for the batch.

d. Test bars did not yield before breaking.

Table 11  
MECHANICAL PROPERTIES OF 75/25 TA/AA-HMDA POLYAMIDE

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		Tensile	
		Strength	Elongation
		ASTM Method	ASTM Method
		D638	D638
Sample	Glass Fiber	M psi	%
Code	%		
10CV27	45	32.1	3.8
ZSK 185	45	31.9	4.3
75/15/10	45	34.5	5.1

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		Flexural		Notched
		Strength	Modulus	Izod
		ASTM Method	ASTM Method	ASTM Method
		D790	D790	D256
Sample		M psi	MM psi	ft-lb/in
Code				
10CV27	45.9	2.01	2.77	
ZSK 185	46.4	1.89	3.45	
75/15/10	53.9	1.77	2.90	

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		Polymer	
		I.V.	
		HDT	(60/40 Solution
		(at 264 psi)	of Phenol/Tetra-
		ASTM Method	Chloroethane
		D648	at 30°C)
Sample		°F	(dl/g)
Code			
10CV27	>580	0.97	
ZSK 185	>580	-	
75/15/10	>580	1.02	

40

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Example B

A series of terpolyamide/Nylon 6,6 blends were prepared. The Nylon 6,6 used was Zytel 101 from Du Pont Company.

The terpolyamide was made in the 10CV Hellcone reactor in the composition of 65/25/10 TA/IA/AA-HMDA. The I.V. of the terpolyamide is 1.02 dl/g. The glass fiber used for this work was PPG 3540 from



PPG Industries. Blends of terpolyamide and Nylon 6,6 with or without glass fiber reinforcement were made by dry mixing without extrusion compounding. All materials were oven dried overnight before molding. The test bars were injection molded on the Boy machine. Physical testing was carried out according to ASTM standard methods. The results are shown in the table below.

Table 12  
MATERIAL PROPERTIES OF NYLON 6,6/  
TERPOLYAMIDE (TPA) (65/25/10) BLENDS

	Nylon TPA Ratio	Glass Fiber %	Tensile	
			Strength	Elongation
			ASTM Method	ASTM Method
			D638	D638
			M psi	%
15	100/0	0	9.07*	72.5*
20	100/0	45	32.8	5.1
	100/0	60	37.4	5.2
25	80/20	0	11.8	4.9
	80/20	45	32.2	4.9
	80/20	60	41.1	5.6
30	60/40	0	12.7	4.5
	60/40	45	34.7	5.0
35	60/40	60	42.0	5.3
	40/60	0	11.8	3.7
	40/60	45	31.8	4.6
40	40/60	60	39.1	4.4
	20/80	0	8.7	2.4
45	20/80	45	32.0	4.2
	20/80	60	38.4	4.7
50	0/100	0	12.6	3.9
	0/100	45	37.7	5.2
	0/100	60	40.2	4.8

\*This sample had yield strength 10,500 psi, yield elongation 5.0%.

Table 12 (Cont'd.)

5	Nylon TPA	Flexural		Notched Izod ASTM Method D256 ft-lb/in
		Strength	Modulus	
		ASTM Method D790	ASTM Method D790	
		M psi	MM psi	
10	Ratio			
	100/0	15.1	0.35	0.8
	100/0	51.7	1.64	4.5
15	100/0	58.2	2.16	5.1
	80/20	17.3	0.41	0.5
20	80/20	49.5	1.55	3.9
	80/20	60.0	2.36	4.8
	60/40	18.9	0.45	0.7
25	60/40	47.5	1.50	4.0
	60/40	63.9	2.42	4.5
30	40/60	19.8	0.52	0.7
	40/60	46.8	1.56	3.7
	40/60	62.6	2.37	4.6
35	20/80	24.0	0.56	0.7
	20/80	49.5	1.75	3.1
	20/80	64.6	2.52	4.6
40	0/100	20.3	0.53	0.8
	0/100	48.6	1.61	3.4
45	0/100	59.0	2.43	4.9

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Table 12 (Cont'd.)

	Nylon	HDT	Water
	TPA	(at 264 psi)	Absorption
	Ratio	ASTM METHOD D648	
		°F	%
5			
10	100/0	163	0.89
	100/0	472	0.50
	100/0	476	0.36
15			
	80/20	179	0.84
	80/20	485	0.42
	80/20	490	0.30
20			
	60/40	225	0.67
	60/40	489	0.35
25	60/40	493	0.25
	40/60	205	0.52
30	40/60	520	0.28
	40/60	517	0.20
	20/80	223	0.36
35	20/80	543	0.22
	20/80	553	0.22
40			
	0/100	230	0.56
	0/100	565	0.29
	0/100	578	0.21

## Example C

65/25/10 TA/IA/AA Terpolyamide with Sodium Hypophosphite:

55 The reactants are loaded into a preheated Helicone reactor. The melt temperature is 171° F. The temperature control is set at 605° F. The agitator is set at maximum rpm (43). The headspace is purged with N2 and then the reactor vents are closed. The heat transfer oil is then applied (320° F). The melt temperature increases to 438° F in sixteen minutes. The reactor pressure is 120 psi. The reactor pressure is

controlled at 120 psi for five minutes as the melt temperature increases to 472° F. The reactor pressure is then vented to 100 psi (10 psi/min). The reactor pressure is controlled at 100 psi as the melt temperature increases to 580° F. The reactor is then vented to atmospheric pressure (20 psi/min). A slow N<sub>2</sub> sweep is applied. The reaction is then stopped immediately. The batch time is forty-five minutes. The resin I.V. is 1.35 dl/g.

With faster reaction rates, reactor pressure should be maintained above 100 psi until sufficient melt temperature is reached to prevent freezing. This is true especially with a higher percent of TA.

#### Example D

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Prepolymer of 75/15/10 TA/IA/AA-HMDA composition having about 0.2 to 0.3 I.V. was first made in the 10CV Helicone reactor (Run No. 10CV 30 to 35). The prepolymer was ground, dried, and then continuously fed to the ZSK-30 twin-screw extruder reactor according to the conditions described on Run Z-225 Table 13. Good color and gel-free pellets were obtained. The polymer had an I.V. of 1.16 dl/g.

#### Example E

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Prepolymer of 85/15 TA/IA-HMDA composition having about 0.2 to 0.3 I.V. was made in the 10CV Helicone reactor (Run No. 10CV 45 to 51). As in the above example, the prepolymer was ground, dried, and then continuously fed to the ZSK-30 twin-screw extruder reactor according to the operating conditions of Run Z-231 Table 13. Good color and gel-free pellets were obtained. The polymer had an I.V. of 0.85 dl/g.

#### Example F

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Prepolymer of 65/25/10 TA/IA/AA-HMDA composition having about 0.12 to 0.16 I.V. was first made on the EGP unit (Run No. EGP-4). The prepolymer was ground, dried, and then continuously fed to the ZSK-30 twin-screw extruder reactor according to the operating conditions of Run ZP-1115 Table 13. Good color and gel-free pellets were obtained. The polymer had an I.V. of 1.01 dl/g.

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#### Example G

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Prepolymer of 65/15/10/10:TA/IA/AA/TMA:HMDA composition having about 0.25 to 0.30 I.V. was made on the EGP unit (Run No. 7835-138). The prepolymer was ground, dried, and then continuously fed to the ZSK-30 twin-screw extruder reactor according to the operating conditions of Run ZP-1205. Good color and gel-free pellets were obtained. The I.V. of the polymer was 1.13 dl/g. The ZSK-30 extruder reactor operating conditions for the above four polymers are shown in Table 13.

Test bars of neat resin and 45% glass-fiber filled resin were injection molded on the Arburg machine. The test results are shown in Table 11.

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Table 13  
ZSK-30 EXTRUDER REACTOR OPERATING CONDITIONS  
FOR POLYAMIDE AND POLY(AMIDE-IMIDE) RESINS

5	Prepolymer Run No.	10CV 30~35	10CV 45~51
	Prepolymer I.V.	0.2~0.3	0.2~0.3
	ZSK-30 Run No.	Z-225	Z-231
10	Material, TA/IA/AA/TMA	<u>75/15/10/0</u>	<u>85/15/0/0</u>
	Barrel Temp., °F		
	Zone 1	400	170
15	Zone 2	505	620
	Zone 3	670	680
	Zone 4	655	668
20	Zone 5	620	640
	Zone 6	600	620
	Melt Temp., °F	615	645
	Screw rpm	100	100
25	Screw Torque, %	38	32
	Polymer I.V., dl/g	1.16	0.85
30	Prepolymer Run No.	EGP-4	EGP-138
	Prepolymer I.V.	0.12~0.16	0.25~0.30
	ZSK-30 Run No.	ZP-1115	ZP-1205
35	Material, TA/IA/AA/TMA	<u>65/25/10/0</u>	<u>65/15/10/10</u>
	Barrel Temp., °F		
	Zone 1	625	400
	Zone 2	645	510
40	Zone 3	610	645
	Zone 4	590	665
	Zone 5	600	600
45	Zone 6	600	600
	Melt Temp., °F	610	610
	Screw rpm	50	200
	Screw Torque, %	20~30	55
50	Polymer I.V., dl/g	1.02	1.13

Table 14

TYPICAL MATERIAL PROPERTIES OF NEAT AND 45% GLASS-  
FIBER FILLED POLYAMIDE AND POLY(AMIDE-IMIDE) RESINS

Sample Code	Glass Fiber %	Tensile		Flexural	
		Strength	Elongation	Strength	Modulus
		M psi	%	M psi	MM psi
Z-225	0	11.5	4.6	23.2	0.56
	45	35.4	5.2	54.8	1.81
Z-231	0	11.6	5.0	17.0	0.51
	45	36.6	4.9	54.5	2.10
ZP-1115	0	13.5	25.5	23.5	0.50
	45	34.5	4.5	50.5	1.75
ZP-1205	0	15.5*	14.6*	23.2	0.50
	45	33.4	3.9	46.6	1.95

Sample Code	Notched Izod ft-lb/in	Tensile Impact ft-lb/in	HDT (at 264 psi) °F
Z-225	1.0	80	256
	2.7	95	>580
Z-231	1.5	55	275
	3.7	165	>580
ZP-1115	1.8	90	235
	1.7	95	540
ZP-1205	1.4	91	220
	2.3	72	527

\*The samples yielded at 16,700 psi yield strength and 6.7% yield elongation.

#### GENERAL PROCEDURE

The salt is prepared as follows: diacid and diamine monomers are charged to a batch reactor, which has a pitched blade turbine and is of suitable temperature and pressure ratings, to provide a homogeneous salt solution. This is typically 425° F to 450° F and 450 to 550 psig. Additional components including water, catalyst, silicone oil end capping reagent, and plasticizer are also introduced in the salt reactor. Water content of the salt can range to 25% by weight. The preferred range is about 13 to 17% by weight.

The salt is metered through a pump and pressure is increased to 1500-5000 psig. The resulting

prepolymer then passes through a preheat zone where temperature is raised from about 425° F to about 450° F to about 550° F to about 625° F. The total residence time here is 25 to 50 seconds. The resulting prepolymer is then flashed through a control valve to give an aerosol mist at a pressure of 0-400 psig and the polymer is then passed through a tubular flash reactor. This reactor is designed to provide a high heat flux to the polymer and has a wall temperature of about 650° F to about 1000° F, melt temperature range is about 500° F to about 750° F through the flash reactor. The total residence time in the reactor is about 0.1 to about 20 seconds, based on feed rate and pressure. (The inherent viscosity (I.V.) is measured in 60/40 phenol tetrachloroethane at 30° C.)

Conveniently, the polymer is injected directly on the screws of the twin-screw reactor denoted as ZSK in Examples H and I, to further increase the molecular weight.

Examples H and I were prepared as described in General Procedure with specific details and results noted hereinbelow.

#### Example H

##### Monomers:

10% hexamethylene diammonium adipate

65% hexamethylene diammonium terephthalate

25% hexamethylene diammonium isophthalate

Water Content: 15% (by weight)

Procedure: The diacids, diamines and water were charged to the salt reactor of room temperature. The initial charge totaled 38 lb (50 g/moles). Additional charges were 7.2 lbs (10 g/moles) each and were fed through lock hoppers as the salt reactor was operated in a fed batch mode. The salt reactor was a 5 gallon stirred tank reactor with a pitched blade turbine, oil jacket, variable speed drive and internal coils.

Once the salt reactor had been charged, it was purged with inert gas and heated to 425° F (218° C). The pressure was set to 480 psig by first allowing the water in the salt to reach its equilibrium pressure and then adjusting with inert gas. In the fed batch operations, the salt saw a range of residence times. They averaged about 100 minutes. Also as a result of the fed batch mode of operation, it was necessary to include a second surge vessel in the salt preparation section. This vessel, which was at 425° F (218° C) and 450 psig, was used to isolate the salt reactor during charge addition.

Upon leaving the salt section, the salt was passed through a 140 micron filter into a two headed positive displacement pump. Temperature through the pump were maintained at 425° F (218° C). Pressure were increased to 1800 psig in the pump. Following the pump, the salt solution was passed through a preheat zone and heated to 600° F (316° C). The pressure prevented vapor formation in the preheater. Residence time in the preheater was 40 seconds.

The salt entered the flash reactor through a research control valve where pressure was reduced from 1800 psig to 400 psig. Wall temperature in the flash reactor were kept at 750° F (399° C) using electrical heaters but the melt temperature ranged from 525° F (274° C) to 612° F (322° C) depending on location in the flash reactor. Pressure in the flash reactor was controlled by a second RCV. Residence time in the flash reactor was estimated at 7.6 seconds. The run had a 141 lb/hr-in<sup>2</sup> specific mass feed rate per unit of cross sectional area.

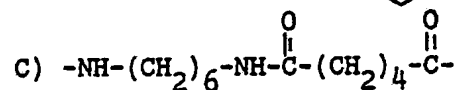
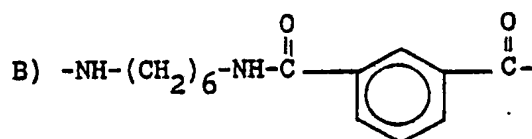
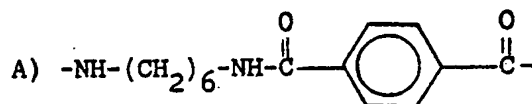
After leaving the flash reactor, our prepolymer had an inherent viscosity (Phenol/TCE) of 0.20 to 0.24 dl/g. It was injected directly onto the screws of the extruder. An open screw design was used to facilitate vapor removal. A screw speed of 200 rpm was used to maintain minimum fill on the screws. Temperatures were 620° F (327° C) in the injection zone but they were dropped gradually to 600° F (316° C) at the die head. Following the extruder, the polymer strand was passed through a water bath and then pelletized. The mean product I.V. was 1.20 dl/g with a standard deviation of 0.09 dl/g over the 6-hour run. Total production was 64 lbs of polymer.

## Example I

5 Monomers: 10% hexamethylene diammonium adipate  
 75% hexamethylene diammonium terephthalate  
 15% hexamethylene diammonium isophthalate  
 10 Water Content: 15% (by weight)  
 Specific Mass  
 Flow: 149 lb/hr-in.<sup>2</sup>  
 15 Residence time: Salt reactor 90 minutes  
 Preheat zone 36 seconds  
 Reactor zone 1.7 seconds  
 Reactor Wall Temp: 700°F Pressure: 100 psig  
 20 Melt Temp: 58±°F to 64±°F  
 Product I.V.: (Phenol/TCE) Tube: 0.40 dl/g ZSK: 1.20 dl/g

## Claims

30 1. An injection molding composition comprising a crystalline polyamide copolymer comprising the following recurring moieties:



50 wherein the mole ratio of A:B:C units is 60-90:35-5:35-5 and from 10 to 60 per cent based on the total weight of the composition of glass fibers, glass beads, mineral fibers or graphite fibers or mixtures of these and wherein the injection molded composition has a heat deflection temperature of 240°C to 305°C, but excluding such compositions wherein the mole ratio of A:B:C units is 60-90:25-5:35-5.

2. A composition according to Claim 1 comprising 20 to 50 per cent of glass fibers, glass beads, mineral fibers, graphite fibers or mixtures of these.

3. A composition comprising a polyamide copolymer as defined in Claim 1 and 1 to 99 weight per cent of the weight of the composition of Nylon 6,6.

55 4. A composition according to any of Claims 1 to 3 in the form of a fiber.

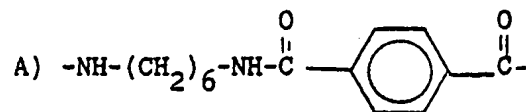
5. A composition according to any of Claims 1 to 3 in the form of a laminate.

6. A composition according to any of Claims 1 to 3 in the form of a molded object.

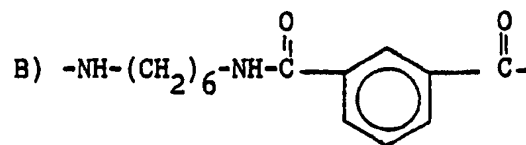


7. An injection molding composition comprising a crystalline polyamide copolymer comprising the following recurring moieties:

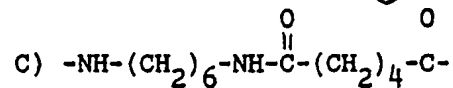
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wherein the mole ratio of A:B:C units is 60-70:25-35:5-15 and from 10 to 60 per cent based on the total weight of the composition of glass fibers, glass beads, mineral fibers or graphite fibers or mixtures of these and wherein the injection molded composition has a heat deflection temperature of 240 °C to 305 °C.